

# Application Data

## **CONTENTS**





## **OPEN-DRIVE COMPRESSORS**

<span id="page-0-0"></span>These compressors are designed to operate with Refrigerants R-407C, R-448A, R-449A, R-22, R-134a, or R-507/R-404A. (See Tables [1](#page-1-1) and 2.)

# **COMPRESSOR PHYSICAL DATA**

#### **Table 1 — Open-Drive Compressors\***

<span id="page-1-1"></span><span id="page-1-0"></span>

LEGEND

**C.L.** — Center Line **ODF** — Outside Diameter Female (in.)

NOTES: \* 5F20 through 5F60 models have been discontinued and application data is for

legacy purposes.<br>† 40°F saturated suction, 105°F saturated discharge, 15°F superheat,<br>0°F subcooling.<br>\*\* Net oil pressure = oil pressure gauge reading – suction pressure. The above<br>oil pressure is typical with mineral or a

## **Table 2 — 5H HFC Compressor Models**

<span id="page-1-2"></span>

\* Compressor unloaders will fully load on elevated oil pressure after compressor start.

† Compressor has no unloading installed. Typically for VFD applications.<br>\*\* Compressor can be applied with external electrical unloading kit<br>5H120-4FI-A.

# <span id="page-2-0"></span>**Operating Requirements**

Satisfactory operation of a reciprocating compressor depends on 3 fundamental requirements:

- 1. Prevention of excess discharge temperature.
- 2. Adequate compressor lubrication.
- 3. A clean and dry system.

# <span id="page-2-1"></span>**Discharge Temperature**

The temperature at the discharge valves within the cylinders is a controlling factor. Some cooling of the discharge gas occurs before reaching the discharge stop valve; thus, when watercooled heads are used, this cooling is greater than it is without water cooling. To prevent excessive temperature at the compressor discharge valves, the following temperatures, when measured immediately following the discharge stop valve, must never be exceeded:



Refer to the Carlyle Compressor Selection program (http://www.carlylecompressor.com) to determine discharge temperature.

# <span id="page-2-2"></span>**High Compression Ratio**

Avoid compressor operation at compressor ratios exceeding those covered in the rating tables, Tables [15](#page-18-0)[-20,](#page-20-0) pages [19-](#page-18-0)[21](#page-20-0). For operating conditions outside the limits shown in these tables, use 2-stage compression. Care must be taken to prevent the compressor from pulling down to levels outside the rating tables.

## <span id="page-2-3"></span>**Suction Gas Superheat**

Excessive suction gas superheat will result in abnormally high discharge temperatures, which must be avoided. When using Refrigerants R-134a and R-507/404A it is recommended that the actual suction gas temperature not exceed the values in Table [3.](#page-2-6) With ammonia, the suction gas superheat must be kept to a minimum to prevent excessive discharge temperatures.

#### <span id="page-2-6"></span>**Table 3 — Actual Suction Gas Temperature Limits (°F) Refrigerants R-134a and R-507/404A**



## <span id="page-2-4"></span>**Keeping Liquid Refrigerant Out of Compressor**

Liquid refrigerant or excessive amounts of entrained liquid particles in suction gas must be kept out of the compressor by proper system design and compressor control. Under operating conditions, presence of unevaporated liquid refrigerant in the compressor tends to break down oil film on cylinder walls, resulting in increased wear and loss of machine capacity.

During compressor operation, proper adjustment of the expansion valve will prevent excessive amounts of liquid from entering the compressor.

During compressor shutdown, gravity, thermal action and refrigerant absorption can result in a refrigerant and oil mixture in compressor crankcase. Gravity flow can be prevented by the use of recommended loops, but thermal action and the absorption of refrigerant by lubricating oil cannot be prevented by piping design.

For the above reasons, the compressor must be controlled during idle times by one of the following methods.

#### MINIMUM PROTECTION

The minimum protection required is shown in Fig. [1.](#page-2-7) Actuated control thermostat energizes crankcase heater and closes the liquid line solenoid valve simultaneously. With crankcase heaters energized, the crankcase temperature is always held above shutdown temperature in the evaporator coil and there will be no refrigerant migration to the crankcase.



**Fig. 1 — Minimum Protection**

<span id="page-2-7"></span>With this type of control, a control relay is required and crankcase heaters have to be energized when the compressor is not operating.

The control relay coil is located in parallel with the liquid line solenoid, and a normally open control relay contact is added in series with the compressor starter and other auxiliary safety devices.

When the thermostat calls for cooling, the solenoid valve opens and control relay is energized. This closes the relay contact and, if other safety devices are in their normal position, compressor will start. Simultaneously, the normally closed compressor auxiliary contact will open, removing crankcase heaters from the circuit.

When the thermostat is satisfied, the solenoid will close and control relay is deenergized. This opens relay contacts and compressor stops. This causes compressor auxiliary contacts to close, energizing crankcase heaters.

Specifications are sometimes written to call for a degree of protection greater than that afforded by the standard method. If this is the case, either single pumpout or automatic pumpdown control may be required.

#### AUTOMATIC PUMPDOWN CONTROL (SEE FIG. [2\)](#page-2-5)

Pumpdown control is the most effective means of compressor control in keeping liquid refrigerant out of the crankcase on system shutdown.



<span id="page-2-5"></span>**Fig. 2 — Automatic Pumpdown Control**

In the basic pumpdown control sequence, the thermostat controls the liquid line solenoid valve to stop or start the flow of refrigerant to the evaporator as required.

The pumpdown control system permits compressor cycling if a system malfunction allows low side pressure to rise. Although this cycling is sometimes considered objectionable, it illustrates need for maintenance attention and provides positive protection against liquid refrigerant accumulating in the compressor crankcase.

Do not use pumpdown control with dry expansion coolers as it may cause frost pinching or freeze-up. Do not use pumpdown control with dry expansion coolers if it is anticipated that there will be short bursts of system operation, as this will result in a gradual loss of oil.

#### SINGLE PUMPOUT CONTROL (SEE FIG. [3](#page-3-2))

Pumpout control is not as effective as pumpdown control in keeping liquid refrigerant out of the crankcase. However, it is usually satisfactory when used with crankcase heaters if pumpdown is not acceptable.



**Fig. 3 — Single Pumpout Control**

<span id="page-3-2"></span>Single pumpout control is similar to pumpdown control, except that a pumpout relay is added, a normally open compressor auxiliary contact is necessary, and energizing of crankcase heaters is required at end of each operating cycle.

With single pumpout control, when the thermostat is satisfied, the compressor pumps down once and stops. It starts again only when the thermostat calls for cooling. In pumpdown control, the compressor cycles only on the low-pressure switch, regardless of thermostat demands.

Do not use pumpout control with dry expansion coolers as it may cause frost pinching or freeze-up.

#### MANUAL PUMPDOWN

The compressor may be controlled manually without the use of pumpdown, or single pumpout control, and without crankcase heaters, provided the system is at all times under control of a qualified operator. The operator will pump down the system by use of manual valves and will keep liquid, suction and discharge valves closed when the machine is not operating.

# <span id="page-3-0"></span>**CARWIN™ Compressor Selection Software**

The Compressor Selection Software (CARWIN™) provides performance data on Carlyle compressors with commonly used refrigerants at air conditioning and refrigeration operating conditions. CARWIN™ calculates performance estimates in a user friendly graphic interface for single-compressor systems.

The Load Match feature in CARWIN™ has the ability to select the compressor(s) per your unique system requirements. Compressor performance estimates generated by the selection software can be output to a PDF or Excel file format.

This software will provide ease of compressor selection and access to performance data information. Use the Carlyle software program CARWIN™ at www.carlylecompressor.com.

## <span id="page-3-1"></span>**Compressor Features and Accessories**

#### WATER-COOLED HEADS AND OIL COOLERS

Water-cooled heads are typically not necessary for R-134a applications within the range of compressor ratings shown in this publication. For R-507/404A at the shaded conditions shown in the compressor ratings tables, water-cooled heads may be necessary if the discharge temperature is greater than 275°F. The discharge temperature will increase with return gas temperature.

When operating conditions are such that suction gas becomes highly superheated and/or the compression ratio is high, it is recommended that an oil cooler be used on the compressor. An oil cooler is required on increased displacement compressors (5H46, 66, 86, and 126) on installations where compressor(s) can be subjected to extended periods of continuous, fully unloaded operation. These periods do not afford sufficient removal of compression and friction heat, and could result in overheating of the running gear, shaft seal and crankcase oil. The addition of an oil cooler removes excessive heat, ensuring increased life expectancy of compressor and components.

*Extended periods of continuous, fully unloaded operation will occur usually on variable-volume installations that use hot gas bypass to maintain conditions under all load situations. Without hot gas bypass, the compressor will usually cycle on the lowpressure switch (or temperature controlling device) giving time for seal, oil and crankcase to cool.*

On multiple-compressor installations where all units are manifolded into one refrigerant circuit, the controls should be designed to cycle off compressors at light loads to put maximum output on the still operative compressor. It is always desirable for the compressor to operate with as many cylinders as possible in loaded condition.

Water-cooled oil cooler package is available from the factory and is easily field installed on all 5 Series compressors. Refer to 5F/H Compressor Ratings to determine when oil coolers are required. These ratings, however, do not indicate oil cooler requirements during periods of extended continuous operation under fully unloaded operation. This should be determined on individual job basis.

Water flow through compressor heads (and water-cooled oil coolers, if used) must be shut off when the compressor is not running to prevent refrigerant vapors from condensing at the compressor during OFF cycles. For this purpose a solenoid valve is recommended in the water supply line to compressor heads.

Values listed in Table [4](#page-3-3) assume a water temperature rise of 30 degrees. Oil cooler and water-cooled heads must be piped in series, with the oil cooler first. Leaving water temperature should be between 100°F and 120°F, with 120°F being maximum allowable temperature. Maximum working pressure for water-cooled heads is 125 psi.

#### <span id="page-3-3"></span>**Table 4 — Minimum GPM Required for Water-Cooled Heads and/or Oil Cooler (Based on 30°F Rise)**



SAFETY RELIEF VALVES

All 5H compressors are equipped with built-in safety relief valves that are factory set to relieve from discharge to suction side of the compressor at a pressure differential of 350 psi.

Safety relief valves that relieve at a 400 psi pressure differential are factory installed on the 5F60 compressor but are not available with smaller 5F compressors.

#### SUCTION STRAINERS

Each 5F/H compressor is equipped with one or 2 suction strainers located in the suction manifold. On new installations, felt filters should be used in suction strainers to trap foreign material left after installation. After 50 hours of use, these felt filters must be removed. See 5F/H Installation Instructions for further details.

#### OIL SAFETY SWITCH

An oil safety switch is provided as standard with all compressors except 5F20 and 5F30. This switch is optional equipment on 5F20 and 5F30 compressors. This switch will shut off the compressor before high oil temperatures or lack of oil causes loss of oil pressure which can result in compressor failure. As a safety feature, this switch must be reset manually after cutout.

#### OIL SEPARATORS

Oil separators in the hot gas discharge line are not recommended for general use. However, there are systems where protection afforded by a separator is desirable, notably systems employing flooded evaporators or refrigeration systems with long system piping. For a more complete discussion see Carrier's System Design Manual.

#### CRANKCASE OIL HEATERS

Crankcase oil heaters are available for all 5F/H compressors. Heaters keep the crankcase warm during off cycles and thus minimize refrigerant absorption in the oil. Refer to the 5F/H Installation Instructions for installation and wiring.

#### INTERCONNECTION OF COMPRESSORS

All 5F/H compressors are furnished with removable handhole cover plates on each crankcase. When field interconnection is desired on 5F40 through 5H86 compressors, cover plates can be removed and replaced by special cover plates with tapped openings. These tapped cover plates have connections for both oil and gas equalizing lines. For interconnection of 5F20 and 5F30 compressors, use the opening for the oil sight glass (see 5F/H Installation Instructions). Cover plates for interconnection are standard equipment on 5F120 and 126 compressors.

Many refrigeration systems utilize oil management components such as an oil separator, oil reservoir and floats. The oil level control float can be installed in the sight glass connection in the 5F/H handhole cover plate.

#### VIBRATION ISOLATORS

A standard vibration isolation package is available for each 5F/H compressor. This consists of a standard rubber-in-shear and compression type mounting that gives an average static deflection of approximately 1/8 in. and provides reasonably good vibration isolation at 1750 rpm.

The use of vibration isolators is recommended for all compressor and condensing units because:

- 1. Transfer of vibration to structure is reduced when the units are installed on upper floors.
- 2. They limit drive shaft misalignment on installations where units are bolted to an uneven concrete floor.

Vibration isolators giving approximately 3/8 in. deflection are available for superior isolation or if the compressor is run at slower speeds. Tables [5](#page-4-0) and [6](#page-5-1) provide an estimated weight distribution on legs of a compressor or condensing unit when used with a normal horsepower motor.

#### MUFFLERS

Four standard mufflers cover the entire model range of 5F/H compressors. It is recommended that these mufflers be installed when compressors are used with remotely located water-cooled or evaporative condensers.

Mufflers are not usually necessary with smaller 5F compressors and their use is recommended only when quiet operation is required.

Each piping package to convert 5H compressor units to condensing units includes a standard muffler of appropriate size.

Pressure drop through mufflers is about 1/2 psi at 40°F suction and 105°F discharge with following loadings: 5 tons with 5F20 muffler, 15 tons with 5F40 muffler, 35 tons with 5H40 muffler and 100 tons with 5H120 muffler.

#### <span id="page-4-0"></span>**Table 5 — Weight Distribution, Condensing Units**



\*Oversize frame.

<span id="page-5-1"></span>**Table 6 — Weight Distribution, Compressor Units**

<b>COMPR</b>		WT DISTR (Ib)	<b>NEMA FRAME SIZE</b>					
		A or D B or C						
<b>Belt Drive</b>								
5F20	115	100	182T, 184T, 213T, 215T					
5F30	140	118	184T, 213T, 215T, 254T					
5F30*	168	145	184T, 213T, 215T, 254T					
5F40	228	165	213T, 215T, 254T, 256T					
5F60	280	210	215T, 254T, 256T, 284T					
5H40	410	305	256T, 284T, 286T, 324T, 326T					
5H60	515	395	286T, 324T, 326T					
5H60*	630	533	324T, 326T, 364T, 365T					
5H80	685	558	324T, 326T, 364T, 365T, 404T					
5H120	1050	728	364T, 365T, 404T					
			<b>Direct Drive</b>					
5F40	210	145	213T, 215T, 254T, 256T					
5F60	245	185	215T, 254T, 256T, 284T, 286T					
5F60*	290	255	256T, 284T, 286T					
5H40	380	275	256T, 284T, 286T, 324TS, 326TS					
5H46	380	275	324TS, 326TS, 364TS, 365TS					
5H80	480	360	286T, 324TS, 326TS, 364TS					
5H60	480	360	365TS, 404TS					
5H66	480	360	286T, 324TS, 326TS, 364TS, 365TS, 404TS					
5H80	690	605	324TS, 326TS, 364TS, 365TS, 404TS					
5H86	690	605	365TS, 404TS, 405TS					
5H120	890	690	364TS, 365TS, 404TS, 405TS, 444TS					
5H126	890	690	405TS, 444TS, 445TS					

LEGEND

**NEMA —** National Electrical Manufacturers Association

\*Oversize frame.

# <span id="page-5-0"></span>**Capacity Control**

The 5F and 5H compressor line incorporates various configurations for cylinder unloading, which are dependent on the compressor model type.

- The 5F compressor family, 5F20 through 5F60, are legacy models and are no longer manufactured by Carlyle. Application data is for legacy purposes.
- The 5F20 and 5F30 pressure unloading models require an external pressure control valve kit (P/N 5F20-A752). The pressure control valve is manually adjusted to direct compressor oil to the unloader power element(s) to unload and load the compressor's cylinders at defined suction pressures for capacity control. (See Table [7](#page-7-0) and Fig. 4.)
- 5F40 through 5H86 legacy models and 5H40 through 5H86 new production pressure unloading models (see Table [2\)](#page-1-2) have a pressure control valve internally installed on the oil pump bearing head. The pressure control valve is manually adjusted to direct compressor oil to the unloader power element(s) to unload and load the compressor's cylinders at defined suction pressures for capacity control. (See Fig. 5 and Fig. 7.)
- For new production 5H40 through 5H86 compressor models (see Table [2](#page-1-2)):
	- Electric unloading models have factory-installed electrical unloading. Unloading solenoid valves are installed on the compressor's bearing head. The bearing head has unloader valves installed that require activation through a solenoid coil. (See Fig. [8](#page-9-0) and [11](#page-11-0).)
	- VFD compressor models do not have unloader elements installed and the cylinders are fully loaded when the compressor is started. A VFD is applied to

operate the compressor speed from 400-1750 rpm. (See Tables [1](#page-1-1) and [2.](#page-1-2))

- Unloaded start compressor models have the unloader elements installed. The unloaded cylinders will load upon compressor start as a result of the compressor oil pressure increasing to activate the unloader power elements, loading the cylinders. (See Table [2](#page-1-2).)
- Legacy 5H40 through 5H86 compressor models that use an external electric unloading conversion kit or apply pressure unloading can be retrofitted with a new electric unloader bearing head, allowing the compressor to be electrically unloaded per Fig. 5. (See Carlyle retrofit instruction 0AHA001431 and retrofit kit 0AHA001431 and retrofit kit P/N 6AH001439.)
- 5H120/126 compressor models:
	- Incorporate a pressure control valve that is internally installed on the compressors oil pump bearing head. The pressure control valve is manually adjusted to direct compressor oil to the unloader power element(s) to unload and load the compressor's cylinders at defined suction pressures for capacity control. (See Table [2](#page-1-2) and Fig. 6 and 7.)
	- Do not have factory-installed electrical unloading but require an external electric unloading conversion kit, P/N 5H120-4FI-A (see Tables [2](#page-1-2) and [8](#page-9-1) and Fig. [8\)](#page-9-0) to unload the compressor.
- Can be applied with a VFD to operate the compressor speed from 400-1750 rpm. (See Tables [1](#page-1-1) and [2](#page-1-2).)

If cylinder head unloading is not preferred, all 5FH compressor models can be applied with a VFD for capacity control. The allowable speed range is 400 to 1750 rpm for non-ammonia models. These compressor models will not have cylinder unloading capability.

The cylinder unloading mechanism is powered by a compressor force-feed lubricating system. This feature assures unloading of all controlled cylinders at starting regardless of the position of the capacity control valve, since suction valves will be held in open position until the lubricating oil pressure reaches its normal operating level. Refer to Fig. [11](#page-11-0) on page [12](#page-11-0) for cylinder unloading sequence.

#### PRESSURE UNLOADING — CAPACITY CONTROL OPERATION

An external adjusting stem is provided to set control point and maintain desired suction pressure. The control point is adjustable from 0 to 85 psig suction pressure. Differential over the complete range at any temperature level is 10.7 psig with Refrigerant 22. A 7-lb spring (for use on 5F40 and larger units) is furnished with the compressor which, when used, results in an adjustable control point from 0 to 50 psig with a 6.8 psig range. (See Fig. 7).

With this arrangement, suction pressure will not drop below the control set point minus the differential within range of capacity steps since the compressor will unload to balance its capacity with evaporator load.

Power elements and valve lifting mechanisms are identical on all 5F/H compressors. However, when using capacity control, various methods are used to activate the power elements.

#### *Major Elements of Control Systems:*

- 1. *Capacity Control Valve:* Function is to raise or lower oil pressure from oil pump in response to refrigerant suction pressure.
- 2. *Power Elements:* Function is to supply power necessary to operate valve lifting mechanism. It is modulated by the capacity control valve.

3. *Valve Lifting Mechanism:* Consists of a sleeve and push pin assembly around each controlled cylinder, designed to hold the suction valve open, or to permit the valve to remain in a normal operating position depending on its actuation by the power element.

## *Principle of Operation of the System*

An increase in suction gas pressure, which requires increased compressor capacity, causes the needle valve to close. Therefore, lubrication oil pressure in power element increases. Increased oil pressure in power element moves the power piston upward and the suction valve discs are allowed to seat.

Table [7](#page-7-0) indicates control oil pressure at which controlled cylinders start to unload and are completely unloaded.

Different points of control pressure on 5F30 are obtained by using springs with different loading rates in the power element.

#### CAPACITY CONTROL FOR 5F40 THROUGH 5H86 (FIG. 5)

## *Major Elements of Capacity Control Systems:*

- 1. *Capacity Control Valve:* Function is to raise or lower the control oil pressure to the hydraulic relay piston in response to refrigerant suction pressure. Increase in suction pressure increases control oil pressure in the hydraulic relay.
- 2. *Hydraulic Relay:* Function is to feed lubrication oil from the oil pump at full pressure in sequence to one or more power elements. Relay is activated by control oil pressure from the capacity control valve.
- 3. *Power Element:* Supplies power to operate the valve lifting mechanism.
- 4. *Valve Lifting Mechanism:* Consists of a sleeve and push pin assembly around each controlled cylinder, designed to hold the suction valve open or to permit the valve to remain in a normal operating position, depending on its actuation by the power element.

## *Principle of Operation of the System*

A decrease in suction gas pressure, which necessitates a decrease in compressor capacity, causes the range spring to open the capacity control modulating valve. This allows control oil to relieve from the hydraulic relay and thus reduces control oil pressure in the relay. With reduced control oil pressure, the spring in the hydraulic relay moves a piston and thus lubrication oil from the oil pump is prevented from flowing to a particular deactivated power element. This relieves oil pressure from the power element, allowing the spring in the power element to move the lifting fork and unload the cylinder. An increase in suction pressure reverses action and loads cylinders.

## 5H120/126 CAPACITY CONTROL (SEE FIG. 6)

This capacity control system is slightly different from the system on 5F40 through 5H86 compressors. Unloaded starting and capacity reduction is obtained by holding open the suction valves of a number of cylinders. For capacity control purposes, a suction-pressure-actuated capacity control valve pilots a hydraulic relay that loads or unloads cylinders in pairs.

## *Major Difference from the 5F40 through 5H86 Capacity Control:*

The hydraulic relay design provides a wider pressure differential between cylinder cut-in and cutout points. The relay is a small, easily removed cartridge rather than an integral part of pump end cover.

#### PNEUMATIC COMPENSATION OF COMPRESSOR CAPACITY CONTROL

Adding a control air line to the external pneumatic control connection permits pneumatic resetting of the control point in accordance with changes in operating conditions. Each pound of change in air pressure resets the control one pound in the same direction. Thus, a one-pound rise in air pressure will cause unloading to begin at a suction pressure one pound higher than the original control point, etc. Figure 5 shows a typical pneumatic control arrangement. All components and installation instructions are field supplied.

## *Control Pressurestats*

Dual pressurestats come factory-installed with some 5F/H compressor models. They are often referred to as high and lowpressure cutouts. Their function is to cut the circuit to the holding coil of the compressor motor starter when pressure setting limits are exceeded.

The high pressurestat has an operating range from 50 to 450 psig with a differential range from 170 to 235 psig (adj). The low pressurestat has an operating range from 20 to 60 psig and a differential range from 60 to 90 psig (adj).

Pressurestat settings should be adjusted on the job to meet particular operating conditions for which the compressor(s) have been selected. Directions for setting these pressurestats are in the 5F/H Installation Instructions.

## *Permanently Unloaded Cylinders*

Operation of an open-drive compressor with its cylinders permanently unloaded requires field modification. 5F60 through 5H66 compressors can operate with one cylinder unloaded; 5H80 through 5H126 compressors can operate with 2 cylinders unloaded. Compressors are modified by removing the suction valve and suction valve springs from the cylinder(s) shown in Fig. [11.](#page-11-0)

<span id="page-7-0"></span>

**Table 7 — Initial and Final Unloading Oil Pressures — 5F20, 5F30**



**Fig. 5 — Capacity Control — 5F40/60; 5H40, 46, 60, 66, 80 and 86**









## 5H40 THROUGH 5H86 FACTORY-INSTALLED ELECTRIC UNLOADING (SEE FIG. [8](#page-9-0) AND TABLE [8](#page-9-1))





<span id="page-9-0"></span>\* See Fig. [11](#page-11-0) for cylinder number designations.

# **Fig. 8 — Unloader Valve/Cylinder Designation (HFC Models)**



<span id="page-9-1"></span>

\* See Fig. 17 for cylinder number designations.

† 5H120/126 requires external unloading conversion kit 5H120-4FI-A.

#### 5H120/126 COMPRESSORS

The following modifications are required to electrically unload 5H120/126 compressors.

- 1. After closing the compressor service valves and reducing refrigerant pressure to the atmosphere, remove pump end bearing head.
- 2. Remove hydraulic relay assembly by removal of two 5/16 in. 18 socket head screws. Make a blank metal disc using a hydraulic relay gasket (5H120-3351) as a guide. Using 1/32 to 1/16 in. thick metal, cut holes in the disc for dowel pins *only*. (Do not cut five 9/32 in. diameter holes.) Reinstall relay assembly using 2 new 5H120-3351 gaskets, one on each side of the metal disc. Torque 5/16 in. socket head screws evenly to 16 to 20 lb-ft.
- 3. Reinstall the bearing head using extreme care not to damage the oil pump tang. Align with recess in the end of the crankshaft. DO not force on.
- 4. Mount solenoid valves and run oil lines. See Fig. [9](#page-10-0) and [10](#page-10-1).
- 5. To minimize vibration, mount the valves on a bracket attached to the compressor.

#### VALVES

The following 3-way valves have been used in the field and are listed as a guide:

- Alco Controls No. 702RA001
- Alco Controls No. S608-1
- Sporlan Type 180





<span id="page-10-0"></span>

<span id="page-10-1"></span>



<span id="page-11-0"></span>12

## <span id="page-12-0"></span>**Motor Selection Data**

Motor selection data based on brake horsepower occurring at design operating condition is usually satisfactory for applications in air conditioning suction temperature range.

Required compressor starting torque is dependent on discharge pressure as well as pressure differential occurring during start-up and is the same for any compressor speed. Values shown in Table [9](#page-13-0) indicate maximum starting torque for R-134a, R-22, and R-507/404A. In most cases, a standard torque motor can be selected because of the partially unloaded starting feature of the 5F and 5H compressors.

In selection of a motor, the required motor starting torque must exceed the compressor starting torque only when the compressor is operating at same speed as the motor. If compressor speed is less than motor speed, as on some belt drive units, the motor starting torque requirements are reduced in proportion to the speed ratio between the compressor and motor because of mechanical advantage available to the motor.

In special applications or systems where there is a large pulldown requirement, the bhp requirement during pull-down may significantly exceed bhp at design conditions. The motor must not be overloaded during pull-down operation. If the motor is sized for pull-down, it will be only partially loaded during design operation and will run inefficiently. Therefore, select a motor that will be optimized for system design requirements and not for pull-down requirements. Two ways for handling this are:

- 1. Install a crankcase pressure regulator in the system to maintain a given saturated suction temperature, thereby controlling bhp requirement, or
- 2. Install a current sensing device so that the motor current draw does not exceed the maximum rated motor current.

# <span id="page-12-1"></span>**Drive Packages**

Table [10](#page-13-1) indicates drive package components for 5F/H standard belt drive packages. Figure [12](#page-14-0) and Tables [11](#page-14-1) and [12](#page-14-2) indicate data for the flywheel used in each of these packages.

# <span id="page-12-2"></span>**Approved Oils**

#### FOR HFCS

Carlyle has approved the following UL-listed refrigerants for use in 5F and 5H compressors: **R-134a, R-404A, R-407A, R-407C, R-407F, R-448A, R-449A, R-450A, R-452A, R-507, and R-513A**.

The following POLYOL-ESTER (POE) are approved oils for HFCs:

Totaline® (see Note 5) P903-1001, 1701 Castrol (see Note 5) E68



All POE oils are very hygroscopic (will readily pick up and retain moisture from the air) and should be used completely once the container is opened. It is extremely difficult to reseal the oil container effectively enough to prevent moisture absorption, which in turn forms damaging acids.

NOTES:

- 1. The use of any non-approved refrigerant may be dangerous and may void the warranty. Contact the Carlyle Compressor engineering department before using any refrigerant or oil not listed in this guide as approved for use in a Carlyle semi-hermetic compressor.
- 2. Using the wrong type or weight of oil for the refrigerant selected will void the warranty.
- 3. Follow the refrigerant and/or oil manufacturer instructions when installing or retrofitting.
- 4. Castrol SW68 (Totaline® P903-1001) is approved for use in Carrier chiller applications as well as Carrier and Carlyle semi-hermetic compressors for air conditioning and medium temperature applications. **Castrol SW68 (Totaline P903-1001) cannot be used in any new low temperature refrigeration applications using Carlyle OEM semihermetic compressors. Castrol E68 is approved for use in Carlyle OEM compressors for low, medium, and high temperature ranges.**
- 5. All HFC/POE applications require a crankcase heater.
- 6. Moisture must be kept below 50 ppm for POE oils.
- 7. In retrofit applications, a high flow oil pump is required.

For HFCs not listed above, please contact Carlyle Engineering for oil recommendations.

#### FOR AMMONIA

## *AMMONIA R-717: CAMCO-717-H Oil For CFCs*

Carlyle has historically approved the following UL listed refrigerants for use in 5F and 5H compressors: R-22, R-500, and R-502 .

The following MINERAL/ALKYLBENZINE are approved oils for CFCs:



NOTE: For CFCs not listed above, please contact Carlyle Engineering for oil recommendations.

<span id="page-13-0"></span>

# **Table 9 — Compressor Starting Torques**

NOTE: R-507/R-404A starting torque values apply to R-448A and R-449A.

# **Table 10 — Belt Drive Packages**

<span id="page-13-1"></span>

# **Table 10 — Belt Drive Packages (cont)**



LEGEND

**PD** — Pitch Diameter (in.)

Compressor shaft diameter before taper begins: 5F20/30=1.0 in. 5F40/60=1.5 in. All 5H=2.0

# Grooves  $F$  to  $G$  of Flywheel D  $\dot{\varphi}$  of Compressor C A A H

**Fig. 12 — Flywheel**

# **Table 11 — Flywheel Data**

<span id="page-14-1"></span><span id="page-14-0"></span>

\*Refer to Fig. [12](#page-14-0).

## <span id="page-14-2"></span>**Table 12 — Flywheel — Compressor Dimensions**



\*Refer to Fig. [12](#page-14-0).

# **BOOSTER COMPRESSORS FOR REFRIGERANT 22 AND 507/404A**

## <span id="page-15-1"></span><span id="page-15-0"></span>**Booster Application Data**

The following data supplements the single-stage compressor application data, and adds information pertaining to booster application only. Refer to the single-stage compressor data for all other information.

# <span id="page-15-2"></span>**Rating Basis**

All booster ratings are given in refrigeration effect and are based on:

- 1. Use of a liquid-suction heat interchanger. All liquid-suction interchangers should have a bypass connection on the liquid side so that adjustment can be made in event that too much superheating of suction gas causes excessive heating of compressor.
- 2. Use of only half of the standard number of suction valve springs per cylinder. All 5F/H compressors are factory assembled with the standard number of suction valve springs; therefore, one-half of the springs per cylinder must be removed in the field for booster applications.
- 3. Booster ratings are based on 1750 rpm compressor speed.

## <span id="page-15-3"></span>**R Factors**

In a multistage compression system, the intermediate or highstage compressor must have sufficient capacity to handle the lowstage (booster) compressor load plus heat added to refrigerant gas by a low-stage machine during compression. Likewise, if an intermediate stage compressor should be used, the high-stage compressor must have sufficient capacity to handle the intermediate stage compressor load plus heat added to the refrigerant gas by an intermediate stage machine during compression.

To assist in the selection of higher stage compressors, Table [13](#page-15-6) presents "R" factors that depict approximate required relationship between stages at various saturated temperature conditions.

To determine the required capacity of a higher stage compressor, multiply lower stage compressor capacity by the proper "R" factor from Table [13](#page-15-6). Any additional loads handled at intermediate pressure must be added to this figure to arrive at the total higher stage load.

# <span id="page-15-4"></span>**Multistage System Pointers**

A staged system is essentially a combination of 2 or more simple refrigerant cycles. In combining 2 or more simple flow cycles to form a staged system for low temperature refrigeration, 2 basic types of combinations are common.

#### DIRECT STAGING

Involves use of compressors, in series, compressing a single refrigerant.

## CASCADE STAGING

Usually employs 2 or more refrigerants of progressively lower boiling points. Compressed refrigerant of low stage is condensed

in an exchanger (cascade condenser) that is cooled by evaporation of another lower pressured refrigerant in the next higher stage.

# <span id="page-15-5"></span>**Safety Factors**

Use of capacity safety factors in selecting booster compressors must be a matter of judgment when making selection.

Factors that have a bearing on satisfactory compressor selections are: accuracy of load estimate, amount of safety factor included in the total load, degree of importance of meeting specified capacity at given condition, temperature level of operation and magnitude of refrigeration load. All of the factors must be recognized when considering the use of a capacity safety factor in selecting a booster compressor.

When a capacity safety factor is used, the compressor is selected at its maximum speed to handle design load plus safety factor (see Fig. [13\)](#page-16-4). Multiplying factors for non-standard speeds are shown in Fig. [14](#page-16-5).

Whether or not added capacity offered by the safety factor is incorporated at once is a matter of judgment. If it is, then the compressor will be operated at maximum speed at the start and any excess capacity achieved will be reflected in faster pulldowns or lower temperatures. It is also a good practice to drive the machine at a speed that will provide slightly more rated capacity than is required by design load. Additional speed-up available will then constitute reserve capacity in the event it is needed. Motors should be sized to run the compressor at maximum speed to forestall any motor changes, should this maximum compressor speed be required in the future.

**Table 13 — Booster "R" Factors**

<span id="page-15-6"></span>

<b>SUCT</b> <b>TEMP</b>	$R-22$ <b>DISCHARGE TEMPERATURE (°F)</b>									
(°F)	$-50$	$-40$	-30	$-20$	$-10$	0	10	20	30	
$-100$	1.261	1.310	1.360	1.410	1.453					
	1.221	1.271	1.319	1.371	1.414					
-90	1.214	1.263	1.313	1.361	1.407	1.448				
	1.175	1.221	1.270	1.321	1.368	1.408				
$-80$	1.170	1.218	1.269	1.315	1.360	1.400	1.434			
	1.129	1.172	1.221	1.271	1.319	1.359	1.394			
$-70$		1.172	1.221	1.269	1.313	1.351	1.388	1.424		
		1.125	1.173	1.221	1.270	1.311	1.348	1.382		
-60			1.178	1.220	1.267	1.303	1.340	1.377	1.406	
			1.125	1.172	1.221	1.263	1.300	1.337	1.367	
-50				1.175	1.219	1.256	1.291	1.329	1.360	
				1.123	1.173	1.217	1.252	1.289	1.319	
-40					1.171	1.209	1.245	1.281	1.311	
					1.126	1.169	1.205	1.241	1.261	
-30						1.160	1.199	1.233	1.265	
						1.121	1.159	1.196	1.227	

Air-Cooled Cylinder Heads

Water-cooled Cylinder Heads



<span id="page-16-4"></span>**Fig. 13 — Booster Compressor Selection Safety Factors**

#### <span id="page-16-0"></span>**Determining Intermediate Pressure**

In application of commercial compressors to staged systems, the lowest total bhp per ton and most economical equipment selection results when using approximately equal compression ratios for each stage. It is also economical to juggle assigned compression ratios to fit available sizes of machines.

<span id="page-16-5"></span>

The use of Fig. [15](#page-17-5) will allow direct determination of proper intermediate pressure that will result in equal compression ratios per stage for a direct 2-stage system. Information in Fig. [15](#page-17-5) is given in terms of saturated temperature instead of pressures, for easier use with compressor ratings.

Existence of a second appreciable load, at some higher suction pressure level, will often dictate the most convenient intermediate pressure.

## <span id="page-16-1"></span>**Gas De-superheating**

Operation of a direct staged system requires cooling of the gas between stages; otherwise, highly superheated discharge gas from low-stage machine would be taken directly into the suction of higher stage compressor and further compression would result in excessive heating of this compressor.

## <span id="page-16-2"></span>**Liquid Cooling**

It is also necessary to employ liquid cooling between stages and increase refrigeration effect of liquid delivered to evaporator to realize rated capacity of booster compressor. Amount of refrigeration expended in cooling liquid between stages is accomplished more economically at the level of high-stage compressor suction than at the level of low-stage suction.

In open-type systems, refrigerant liquid is cooled down to the saturation temperature corresponding to intermediate pressure. In closed-type systems, good intercooler design usually results in refrigerant liquid being cooled down to 10 to 20 degrees above saturation temperature corresponding to intermediate pressure.

## <span id="page-16-3"></span>**Oil Separators and Lubrication**

In cascade-type systems, where evaporators and suction lines are properly designed for oil return to the compressor, oil separators are usually not used.

In direct stage systems, however, oil may tend to accumulate in one of the stages and thus result in lack of lubrication in other machine. By use of oil transfer lines, equalization of oil level between crankcases can be achieved by manual operation at periodic intervals. Automatic control of proper oil return to both compressors is effected by use of a high stage discharge line oil separator, returning oil to high stage machine, and a high side float, connected to high stage machine crankcase, which continually drains excess oil from this crankcase down to the next lower stage compressor.

For booster application, factory oil charge should be drained and replaced with a suitable viscosity oil for low temperature application.



**Fig. 15 — Optimum Intermediate Temperature for 2-Stage Compression (Incorporating Equal Compression Ratios per Stage)**

## <span id="page-17-5"></span><span id="page-17-0"></span>**Control Pressurestat for Booster Application**

The standard dual pressure switch furnished with the 5F/H compressor cannot be used for booster application. Replace it with an appropriate low temperature dual pressurestat that can operate at values shown in Table [14](#page-17-6). Any commercial pressure switch is acceptable.

<span id="page-17-6"></span>

#### **Table 14 — Control Pressurestats for Low Stage Application**

## <span id="page-17-1"></span>**Discharge Valve Springs**

When 5H compressors are used for booster applications where discharge pressure is below 10 psig, the standard discharge valve springs furnished with the machine should be replaced with an equal number of lighter weight springs, Part Number 5H41-1801. No change in discharge valve springs is recommended for 5F compressors.

#### <span id="page-17-2"></span>**Water-Cooled Heads**

Standard 5F/H compressors are not equipped with water-cooled heads but they are available. For applications involving high compression ratios, 5 or above, 5F/H booster compressors should be equipped with water-cooled heads.

## <span id="page-17-3"></span>**Motor Selection Data**

In staged refrigeration systems, the high stage compressor starts first and runs until low stage pressure has been reduced to a predetermined level before the low stage machine starts. With direct staged arrangements, the high stage machine draws gas from the evaporator through low stage machine bypass during this initial period. Size of the selected motor must be related to the maximum condition at which booster compressor can operate.

Compressor may run under heavy loads during periods of high suction pressure, especially on starting when system is warm. To handle these situations the motor must be sized larger than the actual balanced operation brake horsepower indicates, or special attention must be paid to operation of the system when starting initially. Tables [15](#page-18-0)[-20](#page-20-0) give balanced brake horsepower values at 1750 rpm.

If the system is to operate only at a fixed low temperature, it is possible to avoid oversizing of motors provided careful operation is followed when the system is first put in operation.

On applications requiring reduction from ambient conditions to some extremely low temperature, the compression system will be operated at high suction pressures for considerable periods of time. General practice is to drive the high stage compressor with a motor that will operate compressor at the highest expected evaporator temperature. This is generally the "air conditioning" rating of unit. For intermediate or low stage compressors, it is generally sufficient to size motor to take care of double the balance load indicated horsepower plus friction horsepower.

Also consider compressor starting torque requirements when selecting motor for a booster compressor. Starting torque of a motor only large enough to provide required normal operating bhp for booster applications may not be large enough to start the compressor. Recommended minimum motor sizes shown in Table [21](#page-21-8) have been selected to assure adequate starting torque. Actual motor size selected is usually larger, depending on the maximum bhp conditions under which the compressor will run during pulldown or other abnormal operating periods.

It is good practice to select motors with allowance for 10% voltage reduction unless there is a certainty that this cannot occur.

## <span id="page-17-4"></span>**Compressor Starting Torque**

Required compressor starting torque is dependent on the discharge pressure as well as the pressure differential occurring during start-up. Maximum expected torque required during the starting period for 5F/H compressors, used as boosters, is shown in Table [21](#page-21-8) at 2 saturated discharge temperatures.

# **Table 15 — 5F Booster Ratings, R-22**

<span id="page-18-0"></span>

# **Table 16 — 5H 40-66 Booster Ratings, R-22**



LEGEND

**Bhp —** Brake Horsepower<br>**Cap. —** Capacity (Tons)<br>**SDT —** Saturated Suction Temperature (F)<br>**SST —** Saturated Suction Temperature (F)

\* Also referred to as Saturated Intermediate Temperature. † Requires water-cooled heads.

## **Table 17 — 5H 40-66 Booster Ratings, R-22**



# **Table 18 — 5F Booster Ratings, R-404A/R-507**



LEGEND

**Bhp —** Brake Horsepower<br>**Cap. —** Capacity (Tons)<br>**SDT —** Saturated Suction Temperature (F)<br>**SST —** Saturated Suction Temperature (F)

\* Also referred to as Saturated Intermediate Temperature. † Requires water-cooled heads.



#### **Table 19 — 5H 40-66 Booster Ratings, R-404A/R-507**

#### **Table 20 — 5H 80-126 Booster Ratings, R-404A/R-507**

<span id="page-20-0"></span>

LEGEND

**Bhp —** Brake Horsepower<br>**Cap. —** Capacity (Tons)<br>**SDT —** Saturated Suction Temperature (F)<br>**SST —** Saturated Suction Temperature (F)

\* Also referred to as Saturated Intermediate Temperature.

<span id="page-21-9"></span><span id="page-21-8"></span>

<b>COMPR</b> <b>SIZE</b>			<b>MAX COMPR STARTING TORQUE (Ib-ft)</b>	<b>RECOMMENDED MIN MOTOR SIZE HP</b>	<b>FRICTION</b>	
	<b>UNLOADING</b> <b>DURING</b> <b>STARTING</b>		$R-22$	$R-22$		
			Saturated Discharge Temperature (F)	High	<b>Normal</b>	HP* (fhp)
		10 F	30 F	Torque	Torque	
5F20	None	15	21	3	3	0.67
5F30	None	16	24	5	5	0.91
5F40	75%	13	19	5	5	1.15
5F60	66-2/3%	16	24	5	$7 - 1/2$	1.64
5H40	75%	30	45	$7 - 1/2$	10	2.25
5H46	75%	38	56	10	15	2.25
5H60	66-2/3%	37	54	10	15	3.07
5H66	66-2/3%	46	68	15	20	3.07
5H80	75%	41	60	20	20	3.82
5H86	75%	51	75	20	30	3.82
5H120	66-2/3%	65	94	20	30	5.25
5H126	66-2/3%	81	118	30	40	5.25

**Table 21 — Booster Compressor Starting Data**

\* Based on 1750 rpm with 5F/H compressors. Will vary directly with rpm at other speeds.

# **AMMONIA COMPRESSORS**

## <span id="page-21-1"></span><span id="page-21-0"></span>**Ammonia Compressor Models**

Ammonia compressor models are shown in Table [22.](#page-21-10)

#### SAFETY RELIEF VALVES

All 5H compressors are equipped with built-in safety relief valves that are factory set to relieve from discharge to suction side of the compressor at a pressure differential of 350 psi.

## <span id="page-21-2"></span>**Brake Horsepower**

Power input to the compressor is given in brake horsepower. These values are compressor brake horsepower and do not include any losses incurred by the use of a belt drive. Approximately 3 percent should be added to account for drive belt losses.

# <span id="page-21-3"></span>**Liquid Subcooling**

Subcooling the liquid below the condensing temperature by an external means results in improved system performance. If the supply water temperature is low enough, subcooling may be accomplished in a water to ammonia heat exchanger with the same water used to cool the heads. Subcooling can also be accomplished in the subcooling coil of an evaporative condenser.

# <span id="page-21-4"></span>**Compressor Operating Limits**

Operation of ammonia compressors within the limits indicated in the published rating tables will result in trouble-free operation provided the following recommendations and limitations are applied. For physical data, see Table [23;](#page-22-4) for ratings information, use the Carwin performance software and see Fig. [20](#page-26-0) and [21](#page-27-0) on pages [27-](#page-26-0)[28](#page-27-0) of this document.

# <span id="page-21-5"></span>**Discharge Temperature**

The discharge temperature as measured just after the compressor stop valve must never exceed 275°F.

## <span id="page-21-6"></span>**Compression Ratio**

The compression ratio in an ammonia compressor should not exceed 8. On light loading, the compressor must be prevented from pulling down to a low suction pressure which could result in a compression ratio appreciably higher than 8. A compression ratio greater than 8 can result in excessive discharge temperatures and compressor failure.

# <span id="page-21-7"></span>**Suction Gas Superheat**

With ammonia compressors, the suction gas temperature should be as close to saturation as possible, without actual liquid. At high compression ratios, excessive suction gas superheat will result in high discharge temperatures and compressor failure. In practice, the suction gas usually enters the compressor in a slightly superheated condition because of heat gain in the suction line and superheat necessary for satisfactory expansion valve operation. To keep the suction gas temperature rise to a minimum, liquid-suction heat exchangers are never used and the suction line is usually insulated. With ammonia, the suction gas superheat must be kept to a minimum to prevent excessive discharge temperatures.

<span id="page-21-10"></span>

5H41	5H61		5H81 5H121	<b>MODEL</b> <b>NOMENCLATURE</b>	<b>CAPACITY</b> <b>CONTROL</b>	<b>UNLOADER</b> <b>ELEMENTS</b> <b>INSTALLED</b>	<b>SERVICE</b> <b>VALVES</b>	<b>WATER-</b> <b>COOLED</b> <b>HEADS</b>	<b>OPSS</b>	<b>HI/LOW</b> <b>PRESSURE</b> <b>SWITCHES</b>	
v ㅅ	v ⌒	$\checkmark$ ⋏		$-C835$				No			
v ⋏	v ∧	$\checkmark$ ⋏		$-C875$	<b>Electric Unloading</b>	Yes		Yes			
v ㅅ	∧	$\checkmark$ ⌒		$-C915$	Low Torque Start				No	Yes	
$\checkmark$ ∧	∧	$\checkmark$ ⋏		$-C925$	(No Unloading)		Yes	Yes		No	
X	$\checkmark$ ∧	$\checkmark$ ⋏		$-C935$	VFD (No Unloading)			No			
$\checkmark$ ㅅ	v ∧	$\checkmark$ ⋏		$-C945$		No		Yes			
			$\checkmark$ ⋏	$-C934$				No	No.		
			$\checkmark$ ∧	$-C944$				Yes			

**Table 22 — 5H Ammonia Compressor Models**

## **Table 23 — Physical Data**

<span id="page-22-4"></span>

## <span id="page-22-0"></span>**Head Pressure**

Non-condensables such as air must be kept purged from the system and the quantity and/or temperature of the air or water through the condenser set so that the designed condensing pressure will be maintained.

#### <span id="page-22-1"></span>**Discharge Pressure**

The discharge pressure should not exceed 235 psig which corresponds to a saturated condensing temperature of approximately 100°F. Higher saturated discharge temperatures may result in oil breakdown, inadequate lubrication and excessive discharge temperature.

## <span id="page-22-2"></span>**Compressor Design Characteristics and Accessories**

#### OIL COOLER

The 5H ammonia compressors can be equipped with an external, water-cooled, oil cooler. This oil cooler is piped in series with the water-cooled cylinder heads and receives the water flow first.

Cooling of the oil improves the compressor operating efficiency as well as the quality of the oil. The oil temperature will be maintained within the safe limits of 100°F to 120°F when the water quantity and discharge temperature from the heads are as indicated in Table [24.](#page-22-5)

#### <span id="page-22-5"></span>**Table 24 — Water Flow through Heads and Oil Cooler (gpm) Based on 30°F Rise**



#### WATER-COOLED HEADS

Some 5H ammonia compressor models are equipped with watercooled heads. The valve plate is effectively cooled by water flow around the side and top of the heads.

The amount of water required for oil cooler and compressor heads is indicated in Table 19. The temperature of cooling water leaving the heads should be between 100°F and 120°F with 120°F being the maximum permissible temperature.

#### OIL SAFETY SWITCH

An oil safety sensor is standard equipment on all 5H ammonia compressors. This factory-installed sensor must be properly installed and checked for proper operation. This is particularly important because oil tends to collect in the evaporator due to the immiscibility of ammonia and oil.

#### SAFETY RELIEF VALVES

<span id="page-22-3"></span>All 5H ammonia compressors are equipped with safety relief valves to relieve from the discharge to the suction side of the compressor at a pressure differential of 300 psi.

#### HIGH PRESSURE SWITCH

A pressure switch should be installed and set to cut out at a maximum pressure of 240 psi. As a safety control, this pressurestat should be a manual reset type.

#### COMPRESSOR LUBRICATION

Ammonia and oil are practically immiscible, and therefore, very little oil is in circulation in the system. When excess oil is circulated in an ammonia system, this oil will collect in the evaporator(s), resulting in compressor failure from lack of oil.

Therefore, it is essential that the oil level in the crankcase be checked at frequent intervals and oil added when required. The operating oil level in the crankcase of these compressors should be between the bottom of the bull's eye and halfway up the bull's eye. All 5H compressors have the force feed type of lubrication; thus, to ensure proper lubrication, the operating speed should never be less than 400 rpm.

#### COMPRESSOR CAPACITY CONTROL

The 5H ammonia compressor models can be configured with electric unloading or no unloading for variable frequency drive (VFD) operation.

#### *Electric Capacity Control*

When operating with capacity control, three-way solenoid valve(s) are supplied on the compressor and are connected as shown in Fig. [16.](#page-23-1) These valves either supply oil pump pressure to the unloader power cylinder or bleed these elements to crankcase pressure.

During normal operation, when full capacity is required, the appropriate three-way solenoid valves are energized. At this time, the passage from the oil pump to the unloader power elements is open, thus providing oil pressure to the power elements and permitting normal operation of the suction valves.

When capacity reduction is required, the appropriate three-way solenoid valve is de-energized. The oil pump pressure connection is then closed and the oil pressure line from the unloader power elements is open to the crankcase. This relieves the oil pressure from the power elements; thus, they position themselves to hold the suction valves open and unload those particular cylinders.

Based on the compressor model, up to four electrical unloading solenoid valves may be installed on the compressor's bearing head. The unloader valves are normally closed valves and will allow the compressor to start to fully unload upon a compressor start. Therefore the unloader solenoid coil must be energized to load the compressor and sequenced per Fig. [16](#page-23-1) and 17 for proper capacity control.

The 5H ammonia compressor will still utilize the standard power element, unloader sleeve, cylinder sleeve, and lifting fork. But the pressure activated capacity control hardware has been replaced with electrically activated solenoid controls, mounted to the oil pump bearing head and energized via solenoid coils. (See Fig. [18](#page-25-0) and [19.](#page-25-1))

#### *VFD Capacity Control*

The 5H ammonia compressor is approved for VFD operation. The compressor can be configured with no unloading, which means all cylinders will start and operate LOADED only. The compressor's permissible VFD operating range is from 400-1450 RPM for high stage and 400-1600 RPM for low stage.

## <span id="page-23-0"></span>**R Factor**

In a staged compression system, the high stage compressor must have sufficient capacity to handle both the low stage, or booster compressor load, and the heat added to the refrigerant by the low stage compressor.

For THR factors for high stage heat rejection, see Table [25.](#page-26-1) To determine the required capacity of a high stage compressor, multiple the low stage capacity by the "R" Factor corresponding to the saturated discharge temperature. If any additional loads are to be handled by the high stage compressor at its operating suction temperature level, these loads must be added to arrive at the total tonnage capacity of the high stage compressor.



<span id="page-23-1"></span>







**Fig. 17 — Cylinder Unloading Sequence**





<span id="page-25-0"></span>

<span id="page-25-1"></span>

<span id="page-26-1"></span>

# **Table 25 — THR Factors — High Stage Heat Rejection**

NOTE:

1. Multiply the Capacity by the THR Factor to determine Condenser Heat Rejection (btu/hr).



<span id="page-26-0"></span>**Fig. 20 — Multiplying Factors — High Stage Ammonia Multiplier**



<span id="page-27-0"></span>**Fig. 21 — Operating Envelope — High Stage R-717**

# **AMMONIA BOOSTER LOW STAGE COMPRESSORS**

Refrigeration effect values given are based on:

- 1. 10°F superheated suction gas.
- 2. Liquid at the expansion valve being cooled to the saturated discharge temperature of the booster compressor, as when using a flash type intercooler. When the liquid is sub-cooled to some higher temperature, the compressor rating is decreased 2% for each 10°F higher liquid temperature to the evaporator. See Fig. [22.](#page-28-3)
- 3. Three suction valve springs per cylinder. All compressors are factory equipped with size springs and three of these must be removed in the field for booster application.



<span id="page-28-3"></span>

# **R Factor**

In a staged compression system, the high stage compressor must have sufficient capacity to handle both the low stage, or booster compressor load, and the heat added to the refrigerant by the low stage compressor.

For THR factors for high stage and low stage heat rejection, see Tables [25](#page-26-1) and [26.](#page-28-4) To determine the required capacity of a high stage compressor, multiple the low stage capacity by the "R" Factor corresponding to the saturated discharge temperature. If any additional loads are to be handled by the high stage compressor at its operating suction temperature level, these loads must be added to arrive at the total tonnage capacity of the high stage compressor.

# <span id="page-28-0"></span>**Compressor Operating Limits**

Operation of ammonia compressors within the limits indicated in the published rating tables will result in trouble-free operation provided the following recommendations and limitations are applied. For physical data, see Table [23;](#page-22-4) for ratings information, use Carwin performance software and see Fig. [23](#page-29-0) and [24](#page-29-1) in this document.

# <span id="page-28-1"></span>**Discharge Pressure Switch**

For booster operation, an additional discharge pressure switch is usually required to accomplish one or both of the following:

- 1. To automatically control the booster from the interstage pressure.
- 2. To prevent booster compressor operation above a specified interstage pressure to stay within the installed motor horsepower.

# <span id="page-28-2"></span>**Notes for Ammonia Ratings**

- 1. With superheating of the suction gas, compressor rating will be decreased slightly.
- 2. When selecting a condenser, allowance must be made for any pressure drop in the interconnecting hot gas piping.
- 3. Power input to the compressor is given in brake horsepower. These values are compressor bhp and do not include any losses incurred by the use of a belt drive. Approximately 3% should be added to these values to include allowance for belt drive losses.
- 4. Selection of the motor size should be based on the maximum suction and condensing condition under which the compressor will operate. If the motor is selected for the brake horsepower occurring at normal operating suction pressure, it may be seriously overloaded during pulldown or other abnormal periods.
- 5. Water temperature leaving head should not exceed 120°F.
- 6. Operating pressure ratio should not exceed those shown by rating table and curves.
- 7. Capacities and brake horsepower at lower speeds are approximately proportional to rpm.

<span id="page-28-4"></span>

## **Table 26 — THR Factors — Low Stage Heat Rejection**

NOTES:

1. Multiply the Capacity by the THR Factor to determine Mid-Stage Heat Rejection (Btu/hr).



**Low Stage Ammonia Booster Multipliers for Capacity and BHP at 1450 rpm**

<span id="page-29-0"></span>**Fig. 23 — Multiplying Factors — Low Stage Ammonia Booster for Other Than Rated Speeds**



<span id="page-29-1"></span>**Fig. 24 — Operating Envelope — Low Stage R-717**

# <span id="page-30-0"></span>**Accessories**

All 5H ammonia compressors have the following accessory items offered through Carlyle.

- OPSS electronic control, P/N 06DA509570
- Oil Cooler Kit, P/N 5H41-B283
- Discharge Line Muffler, 2-5/8 in. ODF, P/N LM680007
- Unloader Solenoid Coils (for Unloading models only)

See Tables [27-](#page-30-2)[30](#page-30-1) for additional accessories.

## **Table 27 — Crankcase Heaters**

<span id="page-30-2"></span>

\* 5H121 compressor model is not released for production. NOTE: Two (2) crankcase heaters are required for use on 5H81 and 5H121 compressors.





\* Parts required to install a suction and discharge service valve set on

a 5H ammonia compressor.

# **Table 29 — Water-Cooled Cylinder Head Kits (Retrofit only)**



\* 5H121 compressor model is not released for production.

## **Table 30 — Water-Cooled Cylinder Head Hose Kit (See Fig. [28](#page-33-0)[-31](#page-36-0), pages [34-](#page-33-0)[37](#page-36-0))**

<span id="page-30-1"></span>

\* 5H121 compressor model is not released for production.

#### OIL PRESSURE SAFETY SWITCH (OPSS)

Carlyle has approved the following oil pressure safety switch with the 5H ammonia and HFC compressors. The OPSS will mount directly to the oil pump bearing end of the compressor. 5H41 through 5H81 ammonia models and 5H40 through 5H86 HFC models will have the OPSS sensor factory installed, part number 06DA509571 for HFC models and 5H41-7602 for ammonia models. (See Fig. [25](#page-31-2).) The electronic oil safety switch (P/N 06DA509570) is provided as an accessory item that is installed by the OEM. The switch must be properly installed and tested for proper operation as a system pre-start condition.



**Fig. 25 — Oil Pressure Safety Switch**

<span id="page-31-2"></span>The oil safety switch is designed to protect the compressor against the loss of lubrication. The OPSS switch will close the control circuit at compressor startup and allow 120 second oil pressure transitional time delay. The switch will open the control circuit and shut the compressor off when:

- The oil pump pressure drops to a minimum 9 psig above the oil sump pressure after 120 seconds, or
- A time-integrated low differential oil pressure (9 psig) between the oil pump and oil sump pressure that is fluctuating 60% of the time  $\leq$  to 9 psig over a 5 minute rolling window.
- The OPSS will not reset automatically, but must be manual reset provided the differential pressure between the oil sump and pump pressure is above 13 psig.



#### OIL COOLER KIT

All 5H ammonia models will require oil cooling to maintain oil temperatures below 120°F. Kit 5H41-B283 consists of a shell/tube stainless steel heat exchange that mounts directly to the side of the compressor. Hardware is provided that will allow the end user to route tubing from the heat exchanger to the oil pump bearing head. Installation instruction, 99TA516195, will be provided with the kit. (See Fig. [26](#page-32-0).)

The water flow through the oil cooler should be regulated to maintain a return oil temperature to the compressor below 125°F.

The 5H compressor muffler (Fig. [27\)](#page-33-1) installs downstream of the discharge service valve line and functions to reduce the discharge gas pulsations. Failure to install a muffler may result in discharge line joint refrigerant leakage.

NOTE: Only install a muffler compatible for R-717 refrigerant. The muffler should contain no brass, copper, or bronze material. (See Fig. [27](#page-33-1).)



#### SOLENOID COILS

An unloader solenoid coil is required for all 5H models with unloading capability. The table below is a list of qualified solenoid coils that can be applied with the 5H ammonia and HFC compressor.



#### WATER COOLED HEADS

The piping schematics (Fig. [28-](#page-33-0)[31](#page-36-0)) show the location for entering/leaving water connections, which are all 1/2 in. FPT. All piping between cylinder heads is factory installed and pressure tested.

The water flow through the cylinder heads should be regulated to maintain a return oil temperature to the compressor below 125°F and a gas discharge temperature below 250°F.

The associated water flow rates are based on an inlet water temperature of 80°F and a 30°F water temperature rise.

#### <span id="page-31-0"></span>**Precautionary Notes**

The main risks in the use of ammonia as a refrigerant are associated with its toxicity and flammability characteristics. Ammonia gas is severely irritating to wet tissues including eyes, nose, and throat, and it has an unpleasant odor.

The threshold limit value (TLV) for ammonia exposure over an 8-hour period is 25 ppm. This is enough to produce a relatively strong smell without causing eyes to water. For a 15-minute period, the short-term exposure limit (STEL) is 35 ppm.

Only trained technicians with proof of competence should be permitted to work on ammonia refrigeration systems. The standards of competence are defined in BSEN13136 and additional guidance can be found in BSEN378 and the Health and Safety at Work Regulations.

Ammonia is immiscible with mineral oil and draining oil from evaporators is a common maintenance task. This should only be done by trained staff following approved procedures; it requires time and patience, since the cold oil can be very viscous.

Copper, brass, and bronze are easily corroded by ammonia when small amounts of water are present. Pipework is usually steel or stainless steel, and evaporator tubes may be galvanized steel, stainless steel, or aluminum.

## <span id="page-31-1"></span>**5H41, 5H61, and 5H81 Ammonia Compressor Drawings**

See Fig. [32-](#page-37-0)[40](#page-45-0) for drawings of the 5H41, 5H61, and 5H81 ammonia compressors.





**5H41-B283 Oil Cooler Package BOM**

Oil return line

ITEM # PART # QTY DESCRIPTION ITEM # PART # QTY DESCRIPTION KH51ZZ101 1 304 SST Oil Cooler **7** CE20RA101 1 3/8" FPT Tee 5H40-B243 2 Mounting Brackets **8** CA680003 2 3/8" MPT x 1/2" Flare Elbow 5H40-1781 4 3/8"-16 x 3.25" LG Stud **9** CA680004 2 1/2" MPT x 1/2" Flare Elbow AU11AR241 4 3/8" Lock Washer **10** CA63AA101 1 3/8" Hex Head Pipe Plug **AT39AA241 4** 3/8"-16 Hex Nut **12** 5H40-7252 1 Bearing Head Sleeve

<span id="page-32-0"></span>**6** CE01CA110 1 3/8" MPT x 2" LG Nipple





<span id="page-33-1"></span>

<span id="page-33-0"></span>





**Fig. 29 — Water Cooled Head Piping Schematic 5H60/61/66 Single Circuit**





**Fig. 30 — Water Cooled Head Piping Schematic 5H80/81/86 Single Circuit**





<span id="page-36-0"></span>**Fig. 31 — Water Cooled Head Piping Schematic 5H80/81/86 Dual Circuit**



<span id="page-37-0"></span>



**Fig. 33 — 5H40/46 HFC Models**









**Fig. 34 — 5H41 Ammonia and 5H40/46 Models**



**Fig. 35 — 5H61 Ammonia Model**



**Fig. 36 — 5H60/66 HFC Models**









**Fig. 37 — 5H61 Ammonia and 5H60/66 HFC Models**



**Fig. 38 — 5H81 Ammonia Model**



**Fig. 39 — 5H80/86 HFC Models**









NOTE: Dimensions are in. [mm].

<span id="page-45-0"></span>

# <span id="page-46-0"></span>**5H120 and 5H126 Compressor Drawings**

See Fig. [41](#page-46-1) for drawings of the 5H120 and 5H126 compressors and Fig. [42](#page-47-0) for drawings of the 5H121 compressor. Dimensions are shown in inches [mm].



<span id="page-46-1"></span>**Fig. 41 — 5H120/126**



<span id="page-47-0"></span>**Fig. 42 — 5H121**

# <span id="page-48-0"></span>**5F and 5H Legacy Compressor Drawings**

See Fig. [43](#page-48-1)[-49](#page-54-0) for drawings of the 5F and 5H legacy compressors. Dimensions are shown in inches [mm].



<span id="page-48-1"></span>**Fig. 43 — 5F20 Legacy Model**



**Fig. 44 — 5F30 Legacy Model**







**Fig. 46 — 5F60 Legacy Model**



**Fig. 47 — 5H40 Legacy Model**



**Fig. 48 — 5H60 Legacy Model**



<span id="page-54-0"></span>

© 2022 Carrier

Г